

Article

Photovoltaic Panels Temperature Regulation Using Evaporative Cooling Principle: Detailed Theoretical and Real Operating Conditions Experimental Approaches

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Abstract: Solar photovoltaic (PV) applications are gaining a great interest worldwide and dominating the renewable energy sector. However, the solar PV panels' performance is reduced significantly with the increase in their operating temperature, resulting in a substantial loss of energy production and poor economic scenarios. This research contributes to overcoming the PV performance degradation due to the temperature rise. This work involves experimental and theoretical studies on cooling of PV panels using the evaporative cooling (EC) principle. A new EC design to cool the bottom surface of a PV panel was proposed, fabricated, tested, and modeled. A series of experimentation readings under real conditions showed the effectiveness of the method. A steady state heat and mass transfer model was implemented and compared with the experimental data. Fair agreement between the results of the modelling and experimental work was observed. It was found that the temperature of the PV panel can be decreased by 10 °C and the power improvement achieved was 5%. Moreover, the EC helps to stabilize the panels' temperature fluctuation, which results in a better regulation of electrical power output and reduces the uncertainty associated with solar PV systems.

Keywords: PV performance; evaporative cooling; temperature; solar; heat and mass transfer



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1. Introduction

Under the pressure of increasing electrical energy demand and depleting fuels, renewable energy, and especially solar photovoltaic (PV) technology, represent one of the solutions because of the attractive economic and environmental features of these resources. Installing PV panels is becoming essential for governmental, industrial, and domestic sectors for the present and future energy requirements. In 2019, 578 GW_p of solar PV was installed worldwide [1]. However, the actual output of the installed solar PV is drastically degraded due to some environmental factors. Temperature and dust are the main two factors that lower the actual output and badly affect the PV panels' performance. Consequently, many methods have been proposed to manage the temperature problem by cooling the PV panels. The principal cooling methods can be broadly classified as single phase (sensible heat) methods and phase change (latent heat) ones. These include:

1. Cooling by natural and forced air [2,3].
2. Cooling by water [4–6].
3. Cooling by phase change materials (PCM) [7,8].
4. Cooling by evaporation of liquids [9–11].

Recently, S.R. Abdallah et al. used saturated zeolite with water for PV cooling and a 9 °C temperature reduction was achieved [12]. Other techniques were also proposed for cooling PV panels such as thermoelectric cooling [13] and radiative cooling [14]. A comprehensive review of these and other techniques that have been proposed for PV cooling is available in [15–17]. Among these technologies, evaporative cooling (EC)—which is very effective especially in dry climates—has received very little attention. The EC principle is well-known and widely employed in many industrial and residential applications. However, its use for cooling PV panels is very rare. The thermal and electrical efficiency of PV panels using water cooling and active clay pot evaporative cooling methods has been investigated by Rankumar et al. [18]. The advantages of using the evaporative cooling principle are clearly shown. Alami [11] studied the effect of evaporative cooling on the efficiency of the PV modules. His method incorporated a layer of synthetic clay to the back of the module and allowing a thin film of water to evaporate. The results show that a maximum increase of 19.4% in the output voltage and 19.1% in the output power can be obtained.

Drabiniok and Nayer [19] proposed a new PV cooling device based on a bionic evaporation foil made of a porous compound polymer. Details of the fabrication and performance of the proposed cooling device have been highlighted. The results show that a temperature reduction of about 12 °C can be reached. A good potential for further enhancement is reported.

PV EC using the chimney effect integrated with a solar chiller to enhance the performance has been investigated experimentally by Lucas et al. [20]. The results reveal that the PV module temperature difference can reach 8 °C while the average improvement in the module electrical efficiency can be about 7.6% in a typical day with Mediterranean weather. In a recent study, a modified version of the evaporative PV chimney using water sliding was presented, showing an average cooling of the PV module of 15 °C resulting in about 15% improvement in the electrical efficiency [21].

Despite the effectiveness of EC, which explains its wide applications in the industrial sector, the number of studies on using EC in PV cooling is very few, as this review shows. Furthermore, a detailed performance study of this method and its dynamic behavior have not been conducted systematically. Additionally, there are only few experimental studies using EC under real operating conditions. Likewise, there are limited models for simulating simultaneous heat and mass transfer in cooling of PV using EC. Hence, this work attempts to fill these scientific gaps in this field by introducing a new design that implements the evaporation cooling phenomenon to tackle the temperature rise problem in PV panels. This work presents a comprehensive theoretical and experimental study along with a performance study on various parameters that affect the effectiveness of the proposed PV cooling method. This study was carried on under real harsh environmental conditions over several days to ensure the reliability and repeatability of the results. Short-term and long-term results are presented and investigated.

The following sections describe the theoretical heat and mass transfer model and the experimental setup. The obtained experimental and theoretical results are presented and discussed.

2. Modeling

This section presents a model of the heat and mass transfer for evaporative cooling occurring in a rectangular channel with parallel plates used to cool the bottom surface of a PV panel.

2.1. Model Description

The physical model consists of an inclined duct in which the upper surface is a PV panel. The dimensions of the duct are: 3 cm height, 140 cm long and 67 cm width. On the lower side of the duct, water flows on a piece of cloth that functions as a water distributor. Air is blown inside the duct by a fan in the same direction as the water flow (co-current

configuration). A schematic diagram on the considered physical model is shown in Figure 1. The lower surface of the duct is adiabatic. On the top surface, the PV panel is subjected to a uniform solar radiation intensity with heat losses to the ambience. As air flows over the wetted surface inside the duct, water evaporates and cools the air, which, in turn, absorbs the heat from the PV panel body. Since the heat is transferred to the flowing air, the temperature of the PV panel decreases, and electricity production enhances.

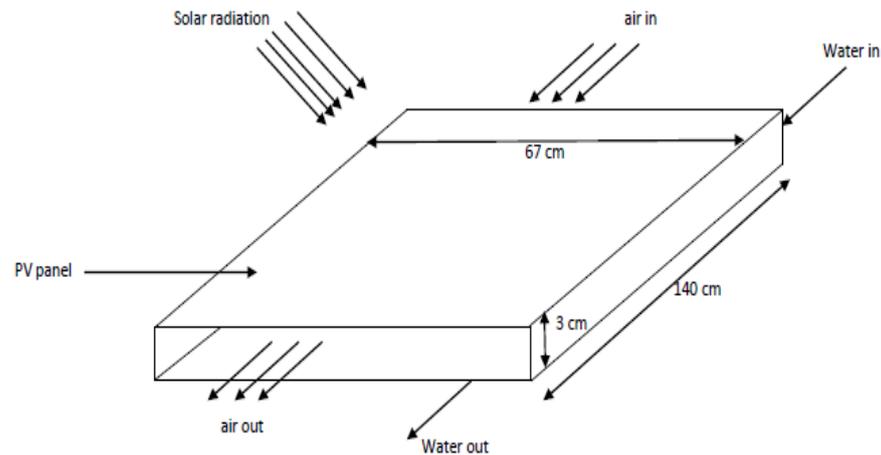


Figure 1. Schematic diagram for the photovoltaic (PV) panel with evaporative cooling.

2.2. Modelling

A uni-dimensional steady state model of heat and mass transfer is used in this work. This model assumes the following: (1) a mass-less layer of saturated gas between the liquid and air exists, (2) the heat and mass transfer coefficients are constants, and (3) the air and water vapor are ideal gases and their specific heat capacities are independent of temperature. The temperatures of air, water, interface saturated layer and PV panel change in the flow direction (x axis). The physical model described schematically in Figure 1 can be simplified and reduced to an inclined channel composed of two parallel plates. The upper surface of the lower plate is covered with a thin layer of water while its lower surface is maintained adiabatic. The bottom surface of the PV panel is cooled with air that is in direct contact with the water layer.

Ambient air enters the channel at known conditions of temperature, humidity, and mass flow rate (T_{ai} , w_i and m_{ia}). It exchanges heat and mass with the water layer as well as the solar PV back surface. The PV panel receives solar radiation G and also exchanges heat with ambience.

The present model is based on a previous model developed by Boulama et al. [22] for the heat and mass transfer between a wetted surface and a gas stream flowing in a duct. It assumes the existence of a very thin film of saturated air between the water and gas streams. The temperature and mass flow ratio for this mass-less layer depend on the axial position but are related by the appropriate saturation equation corresponding to the line for 100% relative humidity on the psychrometric chart. The solar radiation gained by the PV panel and the heat losses to its surrounding are included in the present model.

Energy balances on the PV panel, air, and water layers as well as the water mass balance form the main governing equations of the model. Figure 2 shows a side view of the flow.

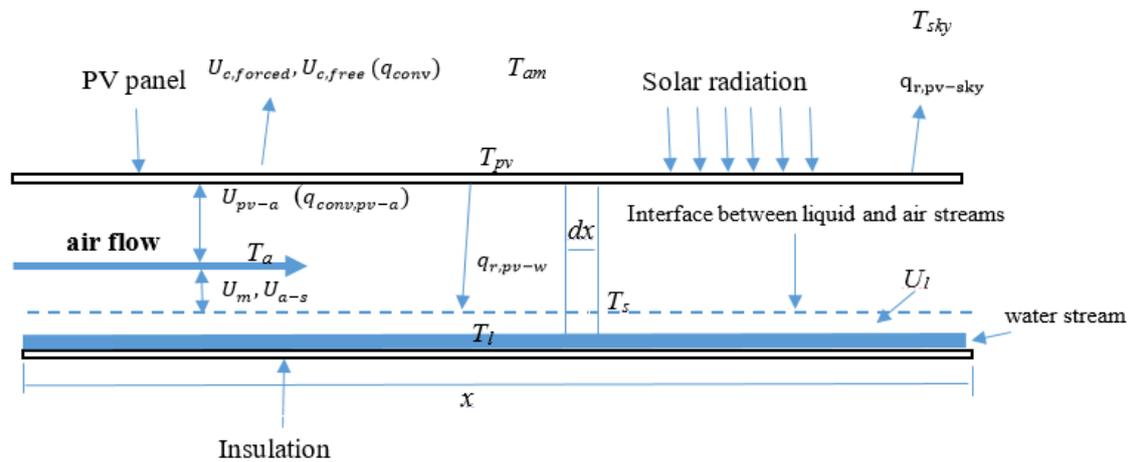


Figure 2. Side view of a heat and mass exchanger with direct contact between a binary gas mixture and a liquid.

Air enters at temperature T_{ai} and exchanges heat with PV panel with heat transfer coefficient U_{pv-a} and with saturation interface layer with heat transfer coefficient U_{a-s} . Mass transfer occurs between air and the interface layer with mass transfer coefficient U_m . Heat transfer also occurs between the water and the interface layer with a heat transfer coefficient U_l . The following equations give the energy balance for each layer.

$$U_{a-s}P(T_s - T_a) + \dot{m}_a \frac{dw}{dx} C_{p,v}(T_s - T_a) + U_{pv-a}P(T_{pv} - T_a) = \dot{m}_a(C_{p,a} + wC_{p,v}) \frac{dT_a}{dx} \quad (1)$$

where P is the panel width and $C_{p,a}$ and $C_{p,v}$ are the specific heat capacity of air and water vapor.

Equation (1) represents the axial change in temperature of flowing air inside the duct. The first term represents the heat transfer between the interface layer and flowing air. The second term concerns the heat transfer associated with the change in the humidity ratio of the flowing air due to mass transfer where \dot{m}_a is the air mass flow rate. The third term gives the heat transfer between the bottom surface of the PV panel and the flowing air. The interface saturation layer reacts with flowing air and water, and its temperature is given by:

$$U_{a-s}P(T_a - T_s) + U_lP(T_l - T_s) = \dot{m}_a h_{fg} \frac{dw}{dx} \quad (2)$$

where h_{fg} is the enthalpy of evaporation of water, and $\frac{dw}{dx}$ is the change of vapor concentration in the flowing air. The water temperature inside the duct changes, as well, with air flow and this is given by the following equation:

$$U_lP(T_s - T_l) = \dot{m}_l C_{p,l} \frac{dT_l}{dx} \quad (3)$$

where \dot{m}_l is the liquid (water) flow rate and $C_{p,l}$ is the liquid specific heat capacity. The change in the water concentration in the flowing air is accounted for by the following equation:

$$\dot{m}_a \frac{dw}{dx} = U_m P (W_s - w) \quad (4)$$

where U_m is the mass transfer coefficient in $\text{kg}/\text{m}^2\text{s}$ and W_s is the saturation humidity evaluated using the following equation [2]:

$$W_s = (7.17 - 0.29T_s + 0.0333T_s^2) 10^{-3} \quad (5)$$

The value of U_m is obtained from the heat transfer coefficient U_{a-s} and Lewis number Le , according to the following equation [22]:

$$Le = U_{a-s} / U_m (C_{p,a} + WC_{p,v}) \quad (6)$$

To deduce the energy balance equation, various energy transfer mechanisms must be identified. First, the convection heat transfer between the PV panel with temperature T_{pv} and ambient air with T_{am} has three components: forced convection between PV panel and ambient air due to wind flow $U_{c,forced}$, free convection or natural convection due to buoyancy effects $U_{c,free}$, and convection between PV panel back surface and air flowing inside the duct U_{pv-a} in the case of the cooled panel. Therefore, the heat convection between PV panels and ambience is:

$$q_{conv} = (U_{c,forced} + U_{c,free}) (T_{pv} - T_{am}) \quad (7)$$

There are wide discrepancies in determining the value of $U_{c,forced}$. Different formulas were proposed in the literature. After systematic investigation and comparing several available correlations in the literature, the following formulas were chosen:

$$U_{c,forced} = 8.91 + 2WS, \quad (8)$$

where WS is the wind speed [23] and

$$U_{c,free} = 1.31 (T_{pv} - T_{am})^{1/3} \quad (9)$$

According to weather data of wind speed obtained from the weather station on the roof of the mechanical engineering department, the wind direction blows mostly from south to north or north to south. This means that the heat transfer by convection from the PV panel will have both components (free and forced) in the wind flow direction and only one component (free convection) in the opposite direction. In the case of the cooled PV panel that is covered from its back by a duct, heat convection occurs just from one side.

Concerning the third component U_{pv-a} , it can be found using the heat transfer correlations after specifying the flow type after determining the value of Reynold's number (Re). The average air velocity inside the duct during the experimentation was around 0.8 m/s. This flow along with duct dimensions results in a Reynold's number in the range $4000 > \text{Re} > 2300$, which corresponds to a transition flow regime. Engineering Equation Solver (EES) software was used to find the value of U_{pv-a} using the procedure "DuctFlow_N", which returns the average Nusselt number and friction factor for constant temperature wall and constant heat flux for the given flow condition in a rectangular duct characterized by Reynolds and Prandtl numbers, length/hydraulic diameter, aspect ratio, and relative roughness.

Hence, the heat transfer by convection between the flowing air and the cooled PV panel will be:

$$q_{conv,pv-a} = (U_{pv-a}) (T_{pv} - T_a) \quad (10)$$

Radiation heat transfer between PV panels and sky temperature is found using the equation given below:

$$q_{r,pv-sky} = \varepsilon_{PV} \sigma (T_{pv}^4 - T_{sky}^4) \quad (11)$$

where σ is Boltzmann's constant, ε_{PV} is the PV panel emissivity and set to be equal to 0.9, and T_{sky} is the sky temperature and is estimated using [24]:

$$T_{sky} = T_{am} - 20 \quad (12)$$

Another radiation heat transfer exists between the cooled PV panel and the wetted cloth inside the duct and is found by:

$$q_{r,pv-l} = \varepsilon_{PV} \sigma (T_{pv}^4 - T_s^4) \quad (13)$$

By considering all the equations, the steady state PV panel temperature is found using the following energy balance equation:

$$G_s(\tau\alpha) = q_{r,pv-l} + q_{r,pv-sky} + q_{conv,pv-a} + q_{conv} \quad (14)$$

where $(\tau\alpha)$ is the optical efficiency of the panel and assumed to equal to 0.9. This is for the cooled PV panel. For the PV panel without cooling, the same equation can be used after removing the first and third terms in the above equation. Finally, it should be noted that this analysis assumes that no electrical load is connected to the panel. If electrical load is connected, another term must be added that accounts for the electrical power that is withdrawn from the PV panel.

3. Experimentation Setup

Figure 3 shows the cooling experiment set up. The panel on the right (no. 2) is the upper surface of a duct of 3 cm depth, 140 cm length and 67 cm width. There is an entrance section (no. 1) and an exit section (no. 3) of lengths equal $5\sqrt{HP}$ and $2.5\sqrt{HP}$, respectively, according to ASHRAE standards 93–77 to ensure uniform distribution of air inside the duct, where H is height of the duct and P is its width. The entrance section is thermally insulated from above to prevent the solar radiation heating up air in that section. The test section (no. 2) is thermally insulated from the two edges and the bottom to decrease heat losses. Five thermocouples (TC) of type K, adhered to the PV panel back surface by aluminum tape, were used to measure the temperature of each panel, five TCs for air temperature and five for water. Each set of TCs was distributed longitudinally. The distance between each two TCs was 28 cm. Three TCs were placed at the end of the test section to measure the humidity of the exit air: two TCs for wet bulb temperature and one TC for dry bulb temperature. The weather station (no. 11) was installed to measure weather data, such as wind speed, ambient temperature, and relative humidity.

The air was blown inside the duct by a fan. Under the PV panel, there was a piece of cloth covering the lower side of the duct. This cloth was used to ensure uniform distribution of water that was fed from a water tank (no. 6), passing through a flow meter (no. 7). The water was supplied to the duct at the top of the test section via holes in a feeding rubber tube and absorbed by the cloth. As air flows inside the duct, it comes into contact with the wetted cloth and initiates water evaporation. Due to evaporation, both water and air temperatures decrease. Additionally, while flowing, air contacts the PV panel back surface and hence absorbs heat from it. This, in turn, reduces the panel temperature and hence increases its efficiency.

The panel on the left-hand side (no. 10) is the reference panel used for the sake of comparison. Five TCs are adhered to the back surface of the reference panel in the same way as the cooled panel. First class SR11-05 pyranometer (no. 5) is used to measure the global solar radiation at the same angle of the PV panels. The wooden frame (no. 9) faces the south and has a slope of 24° , which is—approximately—the latitude of Riyadh. The open-circuit voltage of the two panels was measured directly by an Omega-brand data logger. Three data loggers were used to read the sensors readings and transfer data to a laptop.

The specifications of the PV panels that were used in this experimentation are tabulated in Table 1.

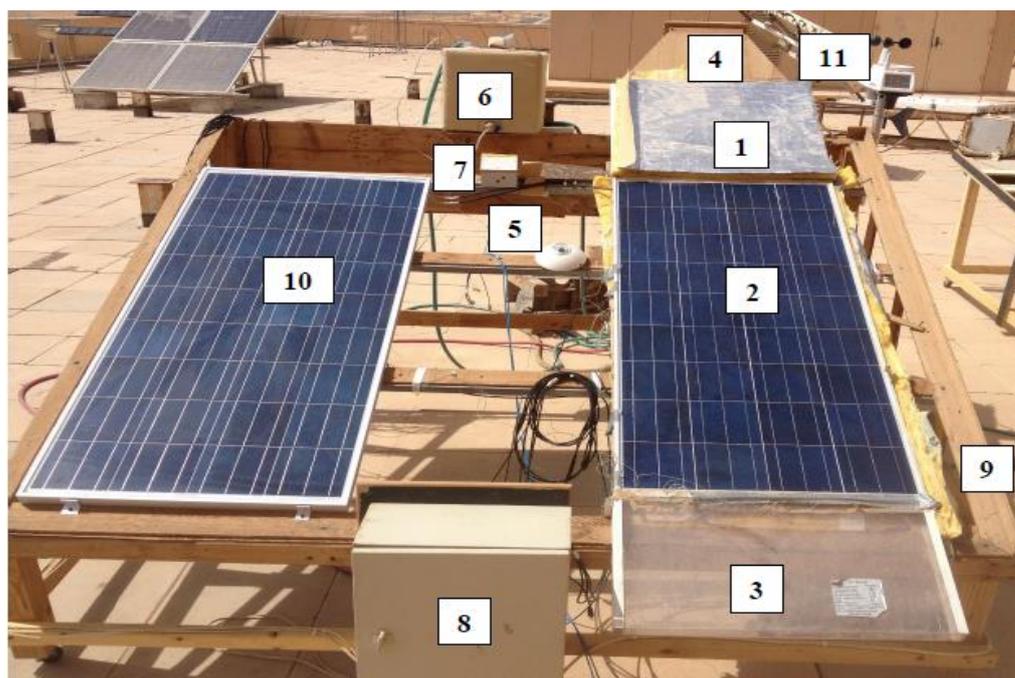


Figure 3. Experiment set up: 1: entrance section, 2: PV panel with cooling, 3: exit section, 4: fan (20W) assembly, 5: pyranometer, 6: water tank, 7: water flow meter, 8: electrical connection box, 9: wooden pool with 24° inclination facing south, 10: reference panel and 11: weather station.

Table 1. PV panel specifications.

Parameter	Value
Rated power (P_{max})	130 W
Volatage at P_{max} (V_{mp})	17.2 V
Current at P_{max} (I_{mp})	7.56 A
Open-circuit voltage V_{oc}	21.6 V
Short-circuit current I_{sc}	8.15 A
Voltage temperature coefficient	−0.3%/°C

4. Results and Discussion

4.1. PV Panels' Temperature

Outdoor experiments were conducted for several days and the main results of the open-circuit voltage and temperature evolutions of the panels with and without cooling are presented and discussed in this section. Comprehensive sensitivity analysis on the effect of the main influencing parameters such as air and water flow rates was conducted using the developed heat and mass transfer model. Additionally, comparison between the experimental and theoretical results is given in detail.

Figure 4 shows the temperature of the two panels over a period from 11:51 to 14:06 on the 27 June. The dotted curves are the actual readings, and the solid ones are the fitted curves.

As the figure shows, the temperature of the hot reference panel (HPV) reached 73 °C, whereas the temperature of the cooled panel (CPV) did not exceed 65 °C. The average difference between the two temperatures is ~10 °C and it reached 12 °C at some instances. Moreover, because of the cooling effect, the fluctuation of the black curve is much less than that of the red one. Figure 5 shows another result for the 30 July.

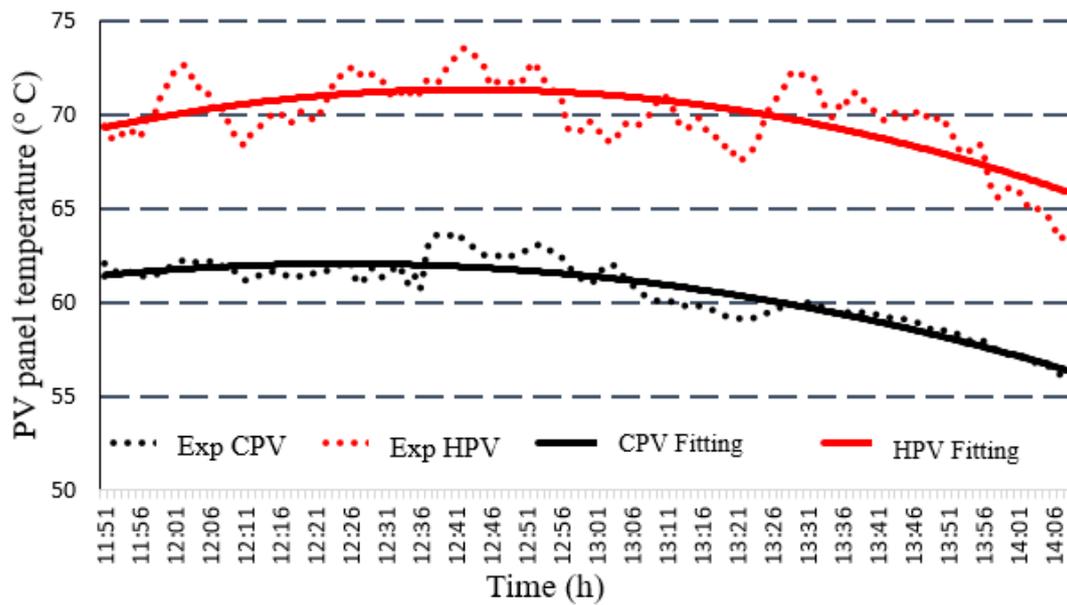


Figure 4. Temperature evolution of the cooled panel (CPV) and reference panel (HPV) at air flow rate = 0.01254 kg/s and water flow rate = 0.0083 kg/s.

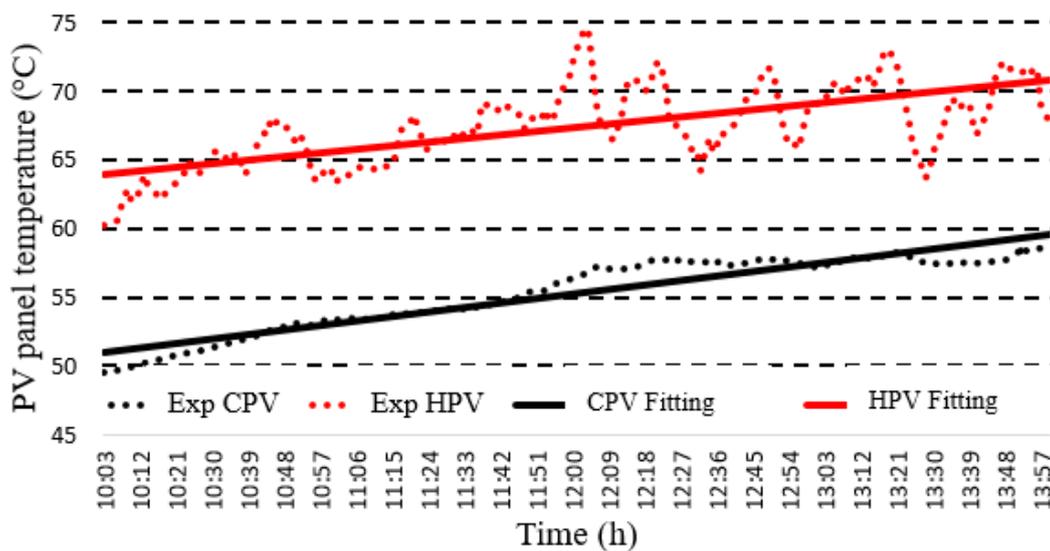


Figure 5. Temperature difference between the cooled panel and reference panel, the 30 July.

4.2. Electrical Power Improvement

The open-circuit voltage V_{oc} of the two panels is shown in Figure 6 where the black dotted and solid curves represent the actual and fitted values of the cooled PV panel, respectively, and the red dotted and solid curves represent the actual and fitted values of the hot PV panel, respectively. The open-circuit voltage of the cooled panel was elevated by ~ 0.7 V at 12:02. Moreover, the voltage of the cooled panel (and hence its power output) is more stable and has less fluctuation than that of the reference panel's voltage.

The stability feature is extremely important from an electric utility point of view because it reduces the solar PV uncertainty and enhances the electric power calculation, such as optimal power flow [25], unit commitment, economic dispatch, generation load balance and quality issues ([26–28]).

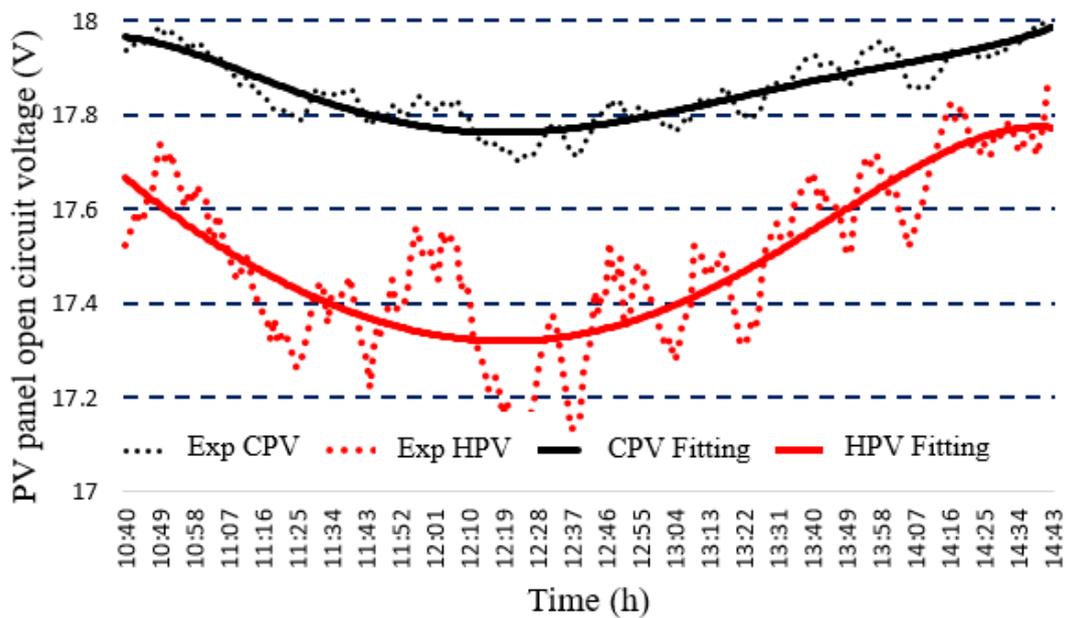


Figure 6. Difference in panels’ open-circuit voltages.

This can be clarified more by referring to Figure 7, which depicts the PV power–voltage curve for different temperatures [29]. As the figure shows, the maximum PV power decreases with temperature and therefore the fluctuation of temperature (up and down as shown in Figure 5) yields a fluctuation in PV voltage (Figure 6) and, consequently, a fluctuation in PV output power.

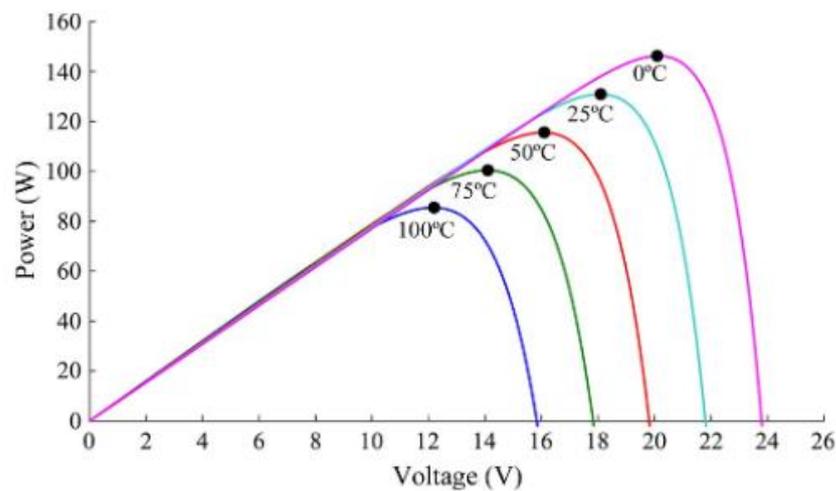


Figure 7. Power–voltage curve of a PV module at different temperatures [29].

Hence, a more stable PV temperature profile (such as the temperature of the cooled panel in Figure 5) results in a more stable PV voltage and output power of solar PV energy sources.

Figure 8 shows the percent of electrical efficiency gain (blue curve with the axis on the right vertical side) associated with the cooling process and the temperature of the two PV panels (the red and black dotted and solid curves with the axis on the left vertical side). The efficiency gain is defined as follows:

$$\text{Efficiency gain \%} = 100 * \frac{\eta_{\text{Cooled PV}} - \eta_{\text{reference PV}}}{\eta_{\text{reference PV}}} \tag{15}$$

where the efficiency of the PV panels is calculated using the well-known formula:

$$\eta = \eta_R [1 - \beta(T_c - T_R)] \quad (16)$$

where η_R is the efficiency at the reference temperature T_R , which is 25 °C, T_c is the actual temperature and β is the efficiency temperature coefficient. The value of β was taken as 0.45% [30]. The average efficiency gain is 6.73%.

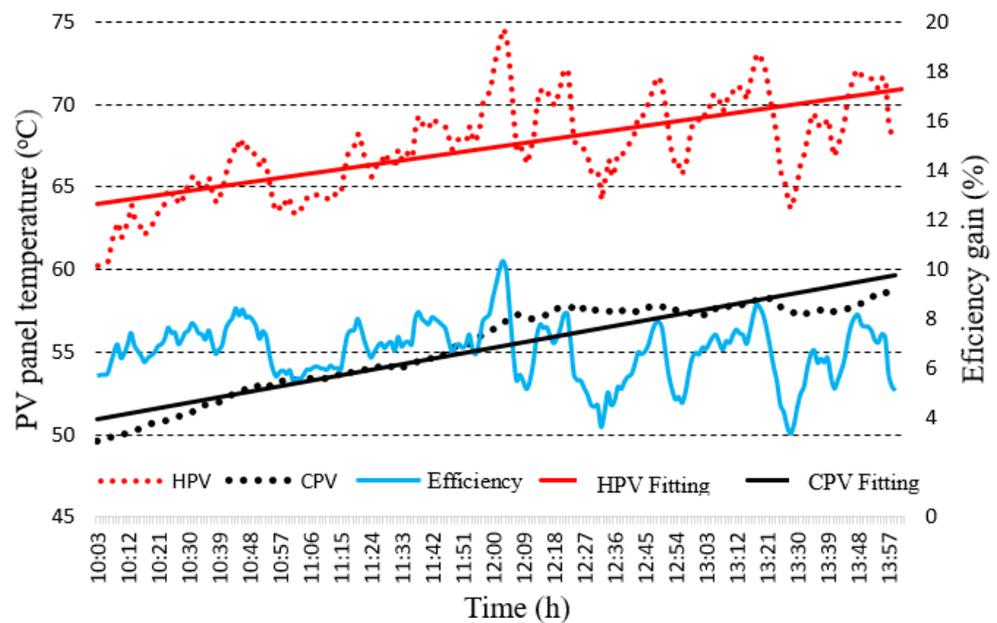


Figure 8. Efficiency gain because of cooling.

It can be seen that the efficiency gain curve looks similar to the HPV temperature curve as the CPV temperature curve has few fluctuations.

4.3. Effect of Water on Air and PV Panel Temperatures

The evaporative cooling process is a complex phenomenon that depends not only on weather conditions such as solar radiation, ambient temperature, and humidity but also on various operating conditions. Water flow rate is among these conditions. Therefore, the effect of water flow rate is presented and discussed in this section.

Figure 9 shows the change in air temperature as it flows inside the duct with different water flow rates. The red and black curves represent the temperature of hot and cold PV panels, respectively. The solid, dashed and dotted blue curves represent the inlet, middle and outlet air temperatures inside the duct, respectively. The green line represents the water flow rate. The experiment was conducted at zero water flow rate before 11:25 and after 13:25. Between these time instants, the water flow rate was fixed at 20 L/h for about 50 min and then at 8 L/h until 13:25. As air enters the duct, it is subjected to two opposite actions: heating from upper side due to solar radiation and cooling from lower side due to the latent heat of the evaporation process and sensible convection heat transfer due to the temperature difference between air and water temperature. Since the heating process effect is greater than the cooling effect, the net effect is an increase in air temperature as it flows inside the duct.

Before the flow of water, the difference between inlet and outlet air temperatures is around 3 °C at hour 9:26 and 6 °C at hour 11:26. However, as water starts flowing, the difference in air temperatures decreases significantly to around 2 °C. Additionally, the cooled PV temperature decreased due to air temperature reduction, which absorbed more heat from the panel.

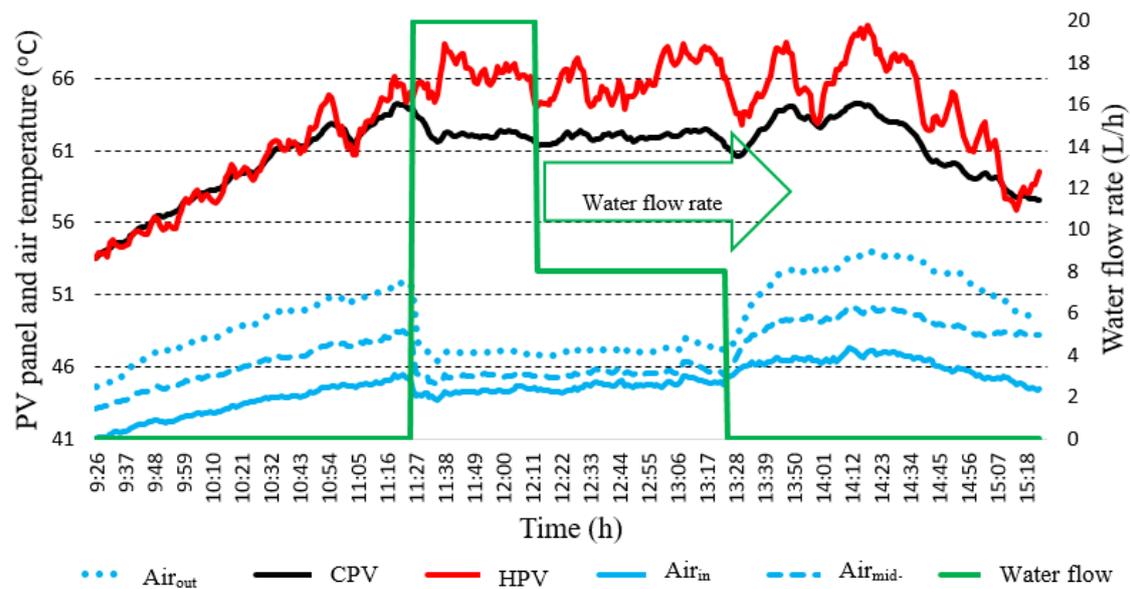


Figure 9. Effect of water flow rate on air and cooled PV temperature, 19 August.

Another important observation is that the change in water flow rate does not have a significant role in the cooling process. It was found that when water flow rate decreased, it did not affect the air and PV panel temperatures. At 11:25, the water flow rate was high > 20 L/h and after 12:12, it decreased to < 10 L/h, but no clear influence was observed. This implies that the cooling process is controlled by the evaporation phenomenon and can be sustained with a very minimal water to wet the lower plate of the duct without the need for water circulation. This lowers the water requirement and calls for deeper study to find the minimum needed water flow rate. Another important observation concerns the effect of the evaporation cooling sustained after stopping the water flow for a considerable period. This is indicated by the difference between the red and blue curve between 13:25 and 15:06. This shows the possibility of utilizing the evaporation cooling in an intermittent manner to further decrease the water and pumping power requirement.

4.4. Comparison between the Experimental and Theoretical Results

This part presents a series of comparisons between the experimental and theoretical results. The proposed model has been used to simulate the temperature distributions of the air, water, and PV panel temperatures under various conditions of solar radiation, air mass flow rate and inlet air and water temperatures.

4.4.1. PV Temperatures

Figure 10 shows the temperature of the cooled PV and the reference PV at the following conditions: $G = 943.8 \text{ W/m}^2$, wind speed (WS) = 1.9 m/s, $T_{ai} = 39.41 \text{ }^\circ\text{C}$, $T_{am} = 38.77 \text{ }^\circ\text{C}$, relative humidity RH = 8.8% and inlet water temperature $T_{li} = 24.43 \text{ }^\circ\text{C}$. The experiment data were taken on 20 June at 11:05 am. As shown, there is a fair agreement between the predicted and experimental results.

It can be seen that the agreement between the simulated and experimental temperatures of the cooled PV panel is better than that of the reference PV panel. The root mean square percentage deviation (RMS%) is 4.68% for HPV and 0.863% for CPV. This may be associated with the effect of wind velocity in which different models and correlations were proposed in the literature to estimate its effect on convection heat loss from the top of PV panels. These models are not generalized for all places and no such models are available specifically for Riyadh. Another factor, which is the wind direction, is not considered in most models of wind effect on PV panels. Since the lower surface of the cooled PV panel is covered by the duct, the wind effect is not as it is in the case of the reference panel.

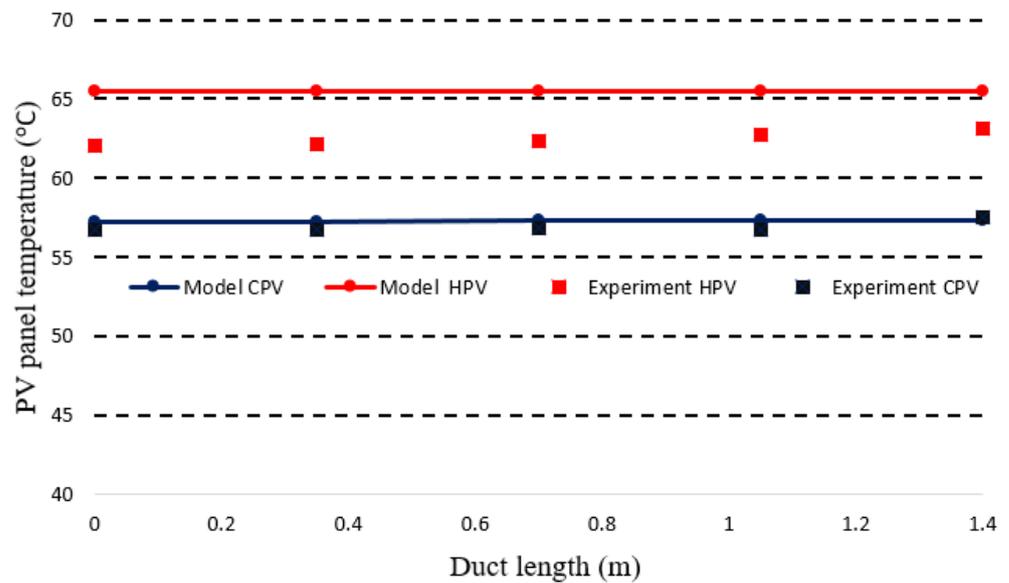


Figure 10. Experimental and simulated cooled and reference PV temperatures on 20 June at 11:05.

Figures 11 and 12 display the temperatures of the cooled PV panel and the reference one for two other different times: at 14:05 on 20 June with RMS% of 3.58% for HPV and 1.66% for CPV and at 13:50 on 22 June with RMS% of 1.18% for HPV and 1.67% for CPV, respectively.

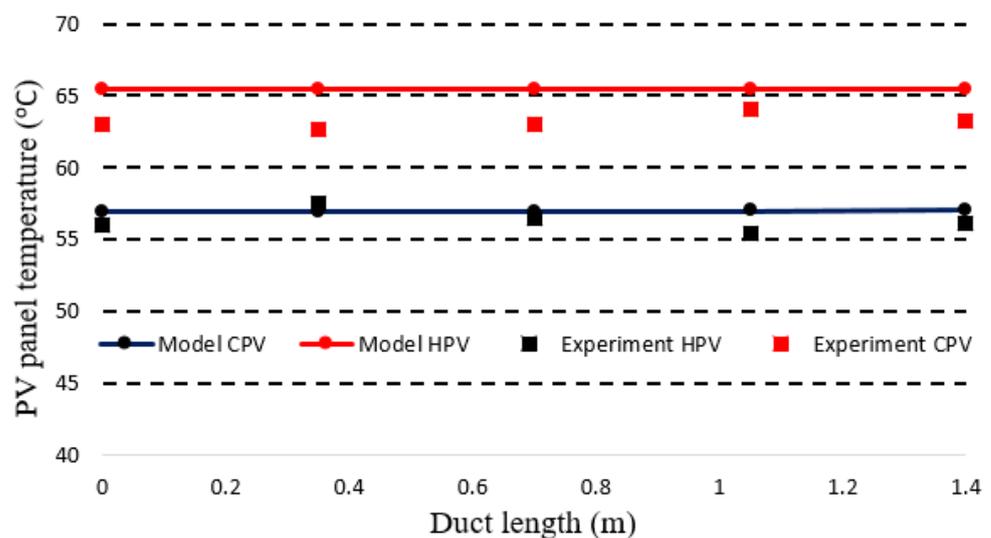


Figure 11. Experimental and simulated cooled and reference PV temperatures on 20 June at 14:05 ($G = 797.88 \text{ W/m}^2$, $T_{am} = 42.25 \text{ }^\circ\text{C}$, temperature (T_{ai}) = $43.72 \text{ }^\circ\text{C}$, inlet water temperature (T_{li}) = $25 \text{ }^\circ\text{C}$, wind speed (WS) = 1.2 m/s , RH = 7.99% , $\dot{m}_{li} = 0.002 \text{ kg/s}$, $\dot{m}_{ai} = 0.0166 \text{ kg/s}$).

It is worth investigating the agreement of the results for a long period. This is beneficial in ensuring the accuracy and correctness of the models.

Figure 13 depicts a comparison between the model and experimental results for a complete experimentation process on 20 June. The developed model was able to accurately predict the temperature evolution corresponding to the hot and cooled PV panels. The difference between the real readings and the model values is because the model was based on the assumption of energy balance but in the actual real case, the PV module does not reach thermal equilibrium due to weather fluctuation [31].

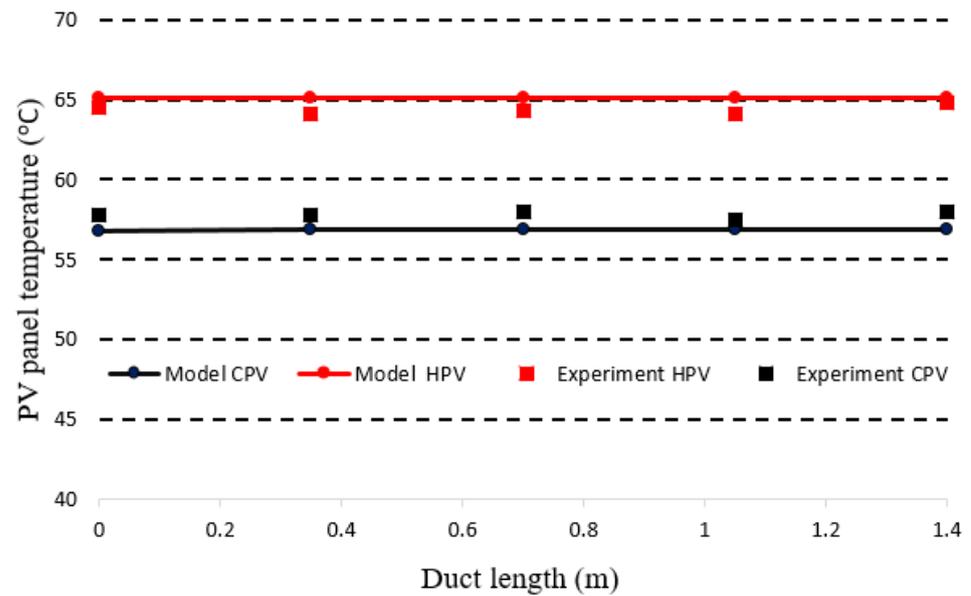


Figure 12. Experimental and simulated cooled and reference PV temperatures on 22 June at 13:50 ($G = 809.412 \text{ W/m}^2$, $T_{am} = 41.75 \text{ }^\circ\text{C}$, $T_{ai} = 43.14 \text{ }^\circ\text{C}$, $T_{li} = 24.47 \text{ }^\circ\text{C}$, $WS = 1.3 \text{ m/s}$, $RH = 7.54\%$, $\dot{m}_{li} = 0.0054 \text{ kg/s}$, $\dot{m}_{ai} = 0.0166 \text{ kg/s}$).

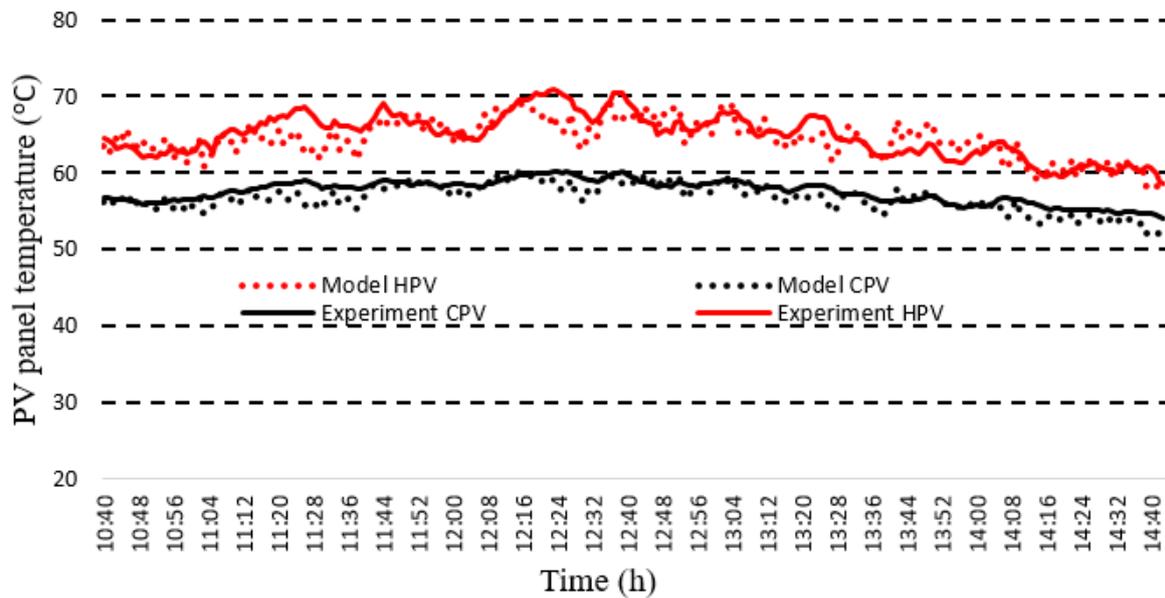


Figure 13. Experimental and simulated cooled and reference PV temperatures on 20 June.

Nevertheless, a very good agreement is observed especially for the cooled PV temperature. The averaged absolute difference (mean absolute error) between the model and experimental values was 1 and 1.8 for the cooled and hot panels’ temperature, respectively.

4.4.2. Water and Air Temperatures

Figure 14 illustrates air and water temperature changes inside the duct from experimental and simulated results. Referring to Figure 2 helps to understand Figure 14. As air flows inside the duct, it is subjected to a cooling process from the lower side and a heating process from the upper side (Equation (1)). The cooling process is due to two effects: the mass transfer from the saturation layer to the air (indicated by the mass transfer coefficient U_m in Figure 2) and the convection heat transfer between the air and the saturation layer

(indicated by the heat transfer coefficient U_{a-s} in Figure 2). The heating process is because of the convection heat transfer between the air and the PV panel (indicated by the heat transfer coefficient U_{pv-a} in Figure 2). Eventually, the net result gives a humid hot air outlet. However, as the duct is thermally insulated from the outside on the lower side, the water stream just reacts with the saturation layer (Equation (3)) by convection heat transfer (indicated by the heat transfer coefficient U_l in Figure 2). The mass transfer from the saturation layer due to evaporation yields a cooling effect on the water stream and, hence, a reduction in its temperature. Apparently, a fair agreement exists between the simulated and experimental results with RMS% of 2.12% for air temperature and 5.8% for water temperature.

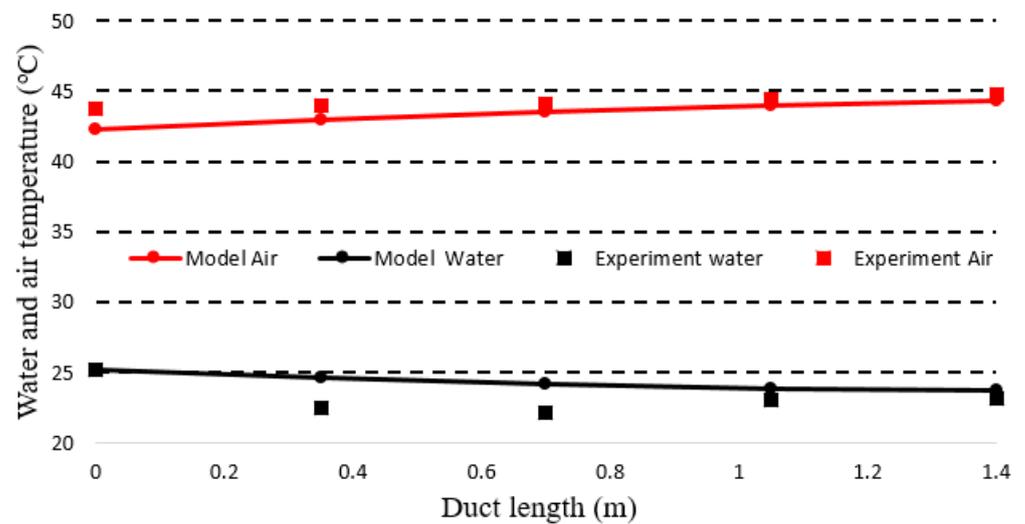


Figure 14. Experimental and simulated air and water temperatures on 20 June at 14:05.

Similar results are shown in Figures 15 and 16 for the same parameters but at different times.

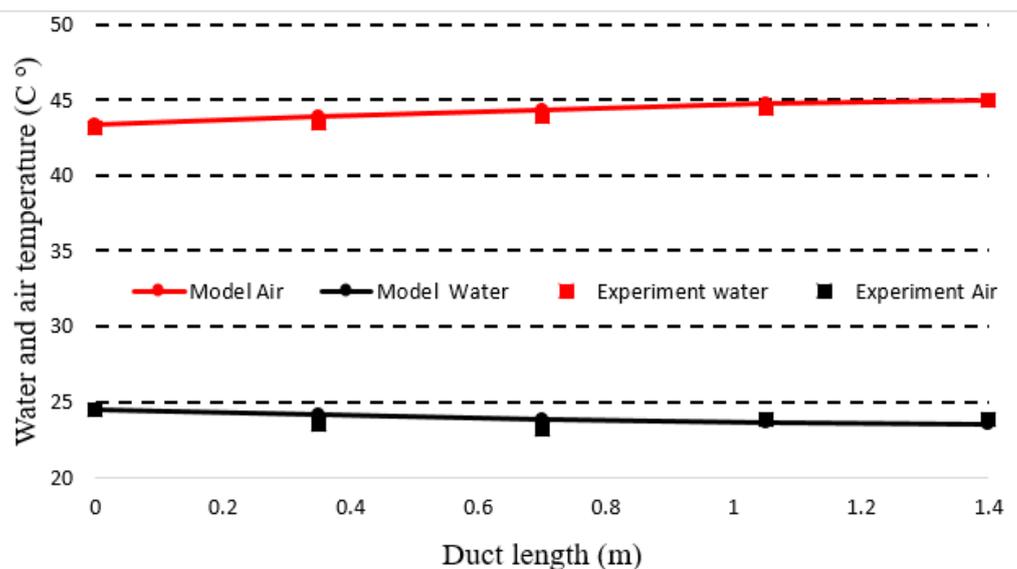


Figure 15. Experimental and simulated air and water temperatures on 22 June at 13:50.

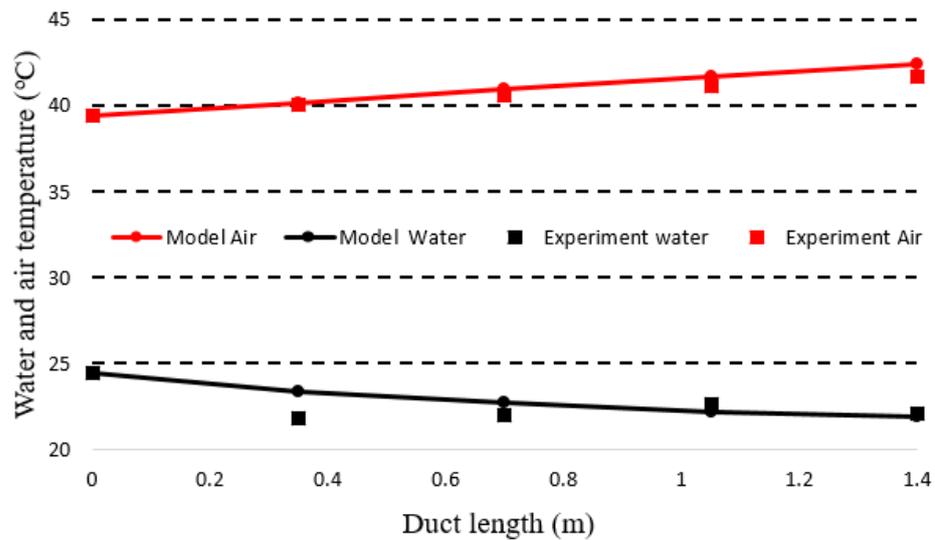


Figure 16. Experimental and simulated air and water temperatures on 20 June at 11:05.

The RMS% is 0.78% and 3.4% for air temperature and 1.9% and 1.58% for water temperature for Figures 15 and 16, respectively.

Finally, the relative humidity of the outlet air can be found using the wet bulb and dry bulb temperatures via the psychrometric chart. For the same conditions of Figure 16, the measured wet bulb temperature was 21.8 °C and the measured dry bulb was 41.63 °C. These values give a relative humidity of around 15%. Comparing this value with the inlet air relative humidity, which was 9.67% (measured), the increase in relative humidity was not significant. This was noted during the whole experimentation process for all days.

4.5. Parametric Study

The theoretical model is further explored to conduct a parametric study to investigate the effect of various factors on the performance of the cooling process. Figure 17 shows the effect of water and air flow rates on the temperature of the PV panel. Both flow rates affect the panel temperature marginally. This agrees with the results presented in Section 4.3.

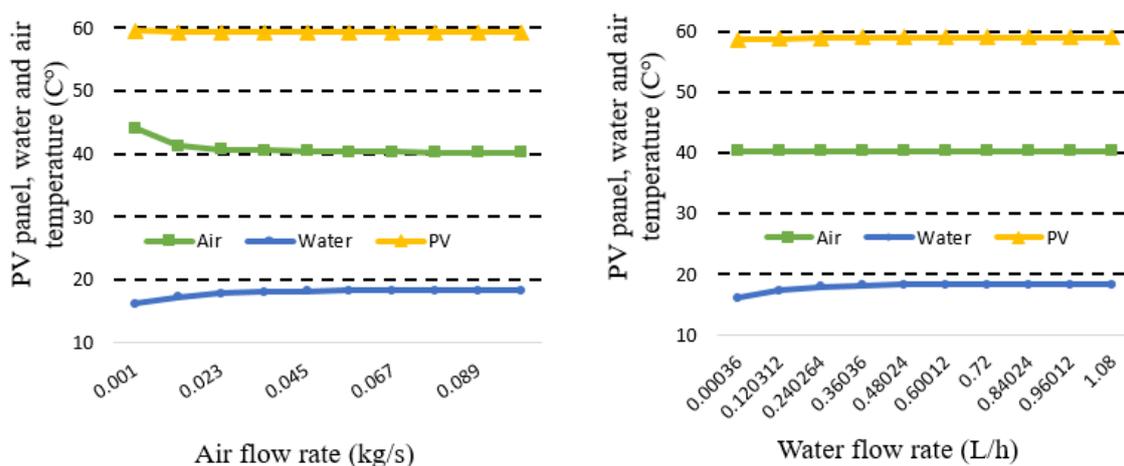


Figure 17. Effect of water and air flow rates on panel's temperature.

Therefore, it can be concluded that very little water is needed for the cooling process, just to wet the lower side on the duct. On the other side, the choice of the smallest air flow rate is a sensitive question since it depends on the pressure losses induced inside the duct.

Figure 18 shows the behavior of the cooling system at different solar radiations. The effect of solar radiation on the PV modules and outlet air temperatures is noticeable, though the water temperature was not affected. At lower solar radiation, the outlet air temperature is lower than the inlet temperature. This implies that the cooling effect between the water and flowing air is larger than the heating effect due to solar energy. As solar radiation increases, its impact is dominant. Another observation is that the difference between the cooled and reference PV modules is larger at high solar radiation ($\sim 9^\circ\text{C}$) and is smaller at low radiation ($\sim 5.5^\circ\text{C}$). Thus, the proposed cooling method is effective at the midday hours when solar radiation is high, and the temperature of the PV panels is elevated.

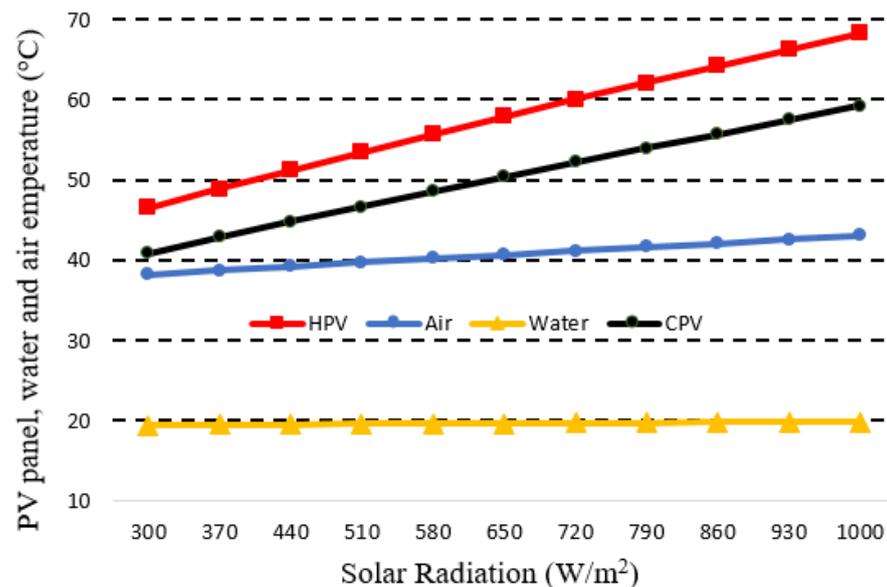


Figure 18. Effect of solar radiation on the cooling system at $T_{ii} = 20^\circ\text{C}$ and $T_{ai} = 40^\circ\text{C}$.

4.6. Fan and Water Pumping Power Consumption

The power consumption of the fan and pump was not measured during the experimental work because these systems were overrated, and the main purpose was to prove the concept and study its technical feasibility. However, the results give some hints regarding this. First, the experiment operation does not require any pumping for water flow inside the duct because the water flows downward due to gravity. Yet, the water needs pumping power to fill the tank before the operation. If there is any adjacent water storage facility (as is the case in many cities in some countries such as Saudi Arabia where every house has a big water tank on the roof), the water can be supplied from this tank. Additionally, as shown in Figures 9 and 17, the water flow rate can be decreased to very small values without affecting the cooling impact and hence it can be deduced that the water requirement for this design is very little. It is just required to wet the cloth piece inside the duct without circulation. Therefore, a few drops of water are enough and the filling process (if any) of the associated tank requires a small pump that will run intermittently with long off-operation and very short on-operation. This discussion implies very low pumping power consumption. Moreover, optimization of the water flow rate can reduce the water quantity and pumping requirement.

Concerning the fan power consumption, the fan power W_f can be calculated using the following equation [32]:

$$W_f = \dot{V}P_D \quad (17)$$

where \dot{V} is the volume flow rate and P_D is the pressure drop. P_D can be calculated as follows [32]:

$$P_D = fL\rho v / (2D_h) \quad (18)$$

where f is the friction factor ($96/\text{Re}$ [32]), L is the duct length (1.4 m), ρ is the air density (1.25 kg/m^3), D_h is the hydraulic diameter of the duct (0.0574 m), and v is the air velocity (0.8 m/s). Using Equations (17) and (18), the value of W_f was found to be equal to 0.0051 watt. Comparing this value by the power gain W_g due to the cooling can be calculated as follows:

$$W_g = \text{efficiency gain} * \text{PV panel rated power} / 100 \quad (19)$$

Efficiency gain is calculated using Equation (15). From Figure 8, the lowest value of the efficiency gain is 3.644%. Putting this value in Equation (19), W_g equals 4.73 watt, which is much larger than the fan power requirement. We can, therefore, conclude that this design is economically feasible.

4.7. Uncertainty Analysis

The uncertainty analysis was conducted to ensure the reliability of the results. The uncertainty analysis was conducted for the thermocouples as they are the main measuring instrument used in this study. The total error of the thermocouples was found to be $1.51 \text{ }^\circ\text{C}$, which is far lower than the readings of the thermocouples during the experimentation process. Detailed calculation can be found in ref. [9].

5. Conclusions

The performance of the PV panels drops significantly with the increase in the operating temperature. Different techniques were proposed to resolve this problem. Using evaporative cooling in dry climates such as Riyadh is a simple and very effective way to reduce the PV panels' temperature. A sequence of evaporative cooling experimentations was conducted and the enhancement in electrical power was investigated by measuring the open-circuit voltage. The experimentation process was carried out for a long time in the summer under real environmental conditions (outdoor test). It should be noted that these experiments were carried out under real outdoor environmental conditions in very a hot climate; on the actual normal size of PV panels at actual inclination and mounted for several days. The temperature of the PV panel was decreased by more than $10 \text{ }^\circ\text{C}$ and power improvement reached 5%. However, the cooling performance was stable and showed a competitive achievement. Additionally, a theoretical model on the heat and mass transfer in a wetted channel was developed and systematically validated using the experimental data. Fair agreements have been found between the theoretical and experimental results. The obtained results show that the evaporative cooling process is effective, economically feasible, and the water quantity required is very little (just to ensure a uniform wetting of the surface). Furthermore, an important observation is that the evaporative cooling reduced the PV temperature fluctuation and thus improved the electrical output stability. This feature is highly desired in electrical power systems with high solar PV energy penetration.

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Nomenclature, Subscripts and Special Symbols

C_p	specific heat at constant pressure [$\text{J kg}^{-1} \text{K}^{-1}$]
CPV	cold PV panel (cooled panel)
D_h	hydraulic diameter
EXP	experimental data
f	friction factor
G	solar radiation [Wm^{-2}]
H	height [m]
h	specific enthalpy [J kg^{-1}]
h_{fg}	specific enthalpy of evaporation [J kg^{-1}]
HPV	hot PV panel (reference panel)
L	length [m]
Le	Lewis number
\dot{m}	mass flow rate (kg s^{-1})
P	width [m]
P_D	pressure drop [Pa]
q	heat flux [Wm^{-2}]
Re	Reynold's number
RH	relative humidity
ρ	density [kg/m^3]
T	temperature [$^{\circ}\text{C}$]
TC	thermocouples
U	coefficient of heat transfer [$\text{Wm}^{-2} \text{K}^{-1}$]
U_m	coefficient of mass transfer [$\text{kgm}^{-2} \text{s}^{-1}$]
V	voltage [V]
\dot{V}	volume flow rate [m^3/s]
v	air velocity [m/s]
W_s	saturation humidity (kg of vapor/kg of air)
W_f	fan power
W_g	power gain
WS	wind speed ms^{-1}
x	axial coordinate (m)

Subscripts

am	ambient temperature
c	actual
$conv$	convection
i	inlet conditions
l	liquid (water)
mp	maximum power
oc	open circuit
pv	PV panel
R	reference
r	radiation
s	saturated layer
sc	short circuit
v	water vapor

Special Symbols

β	PV panels efficiency temperature coefficient
ε	emissivity coefficient
ρ	density [kg/m^3]
σ	Boltzmann's constant
η	efficiency
$\tau\alpha$	optical efficiency

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